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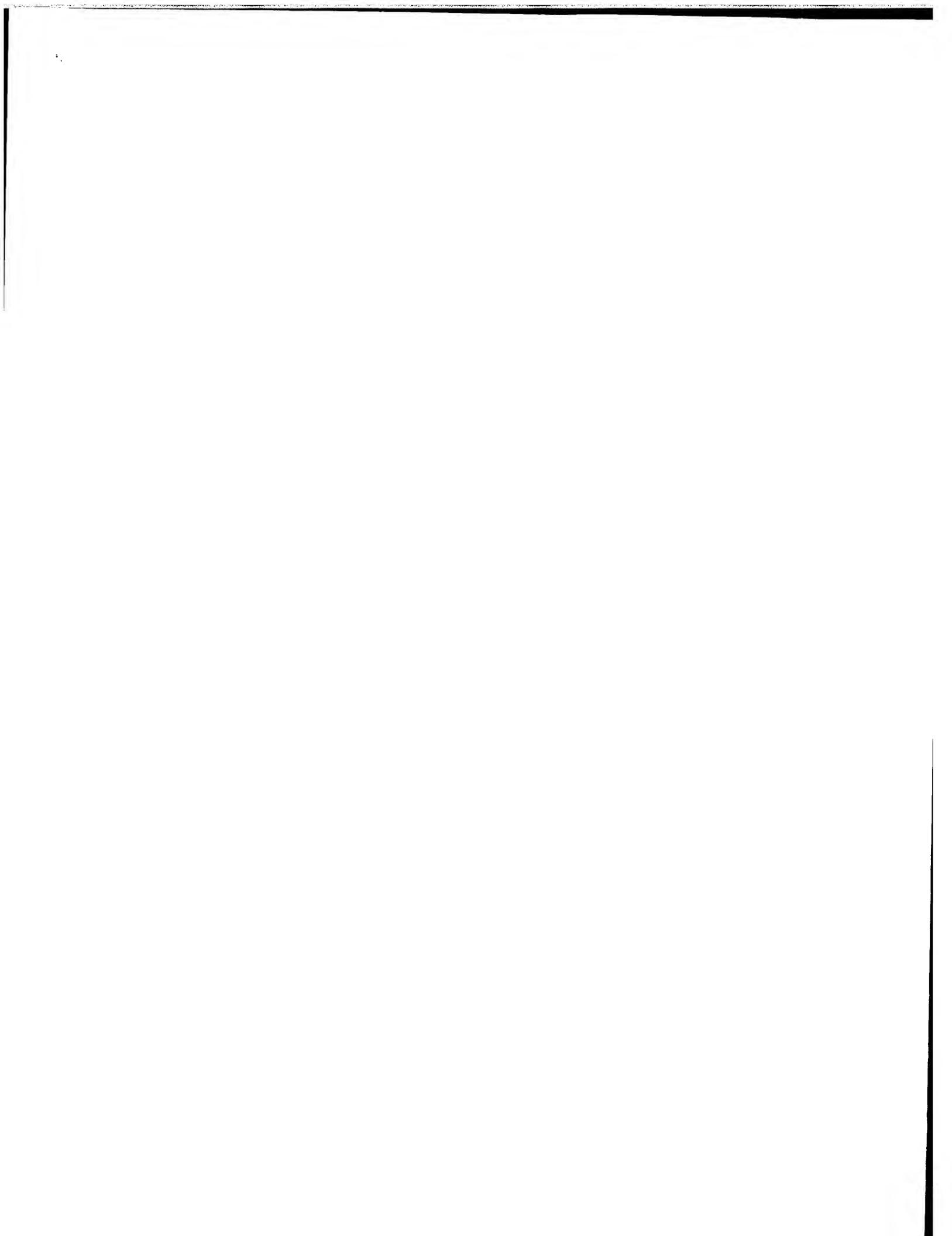
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Der Präsident des Europäischen Patentamts;
Im Auftrag

For the President of the European Patent Office
Le Président de l'Office européen des brevets
p.o.

R C van Dijk





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Cooling module and reactor for carrying out an exothermic reaction

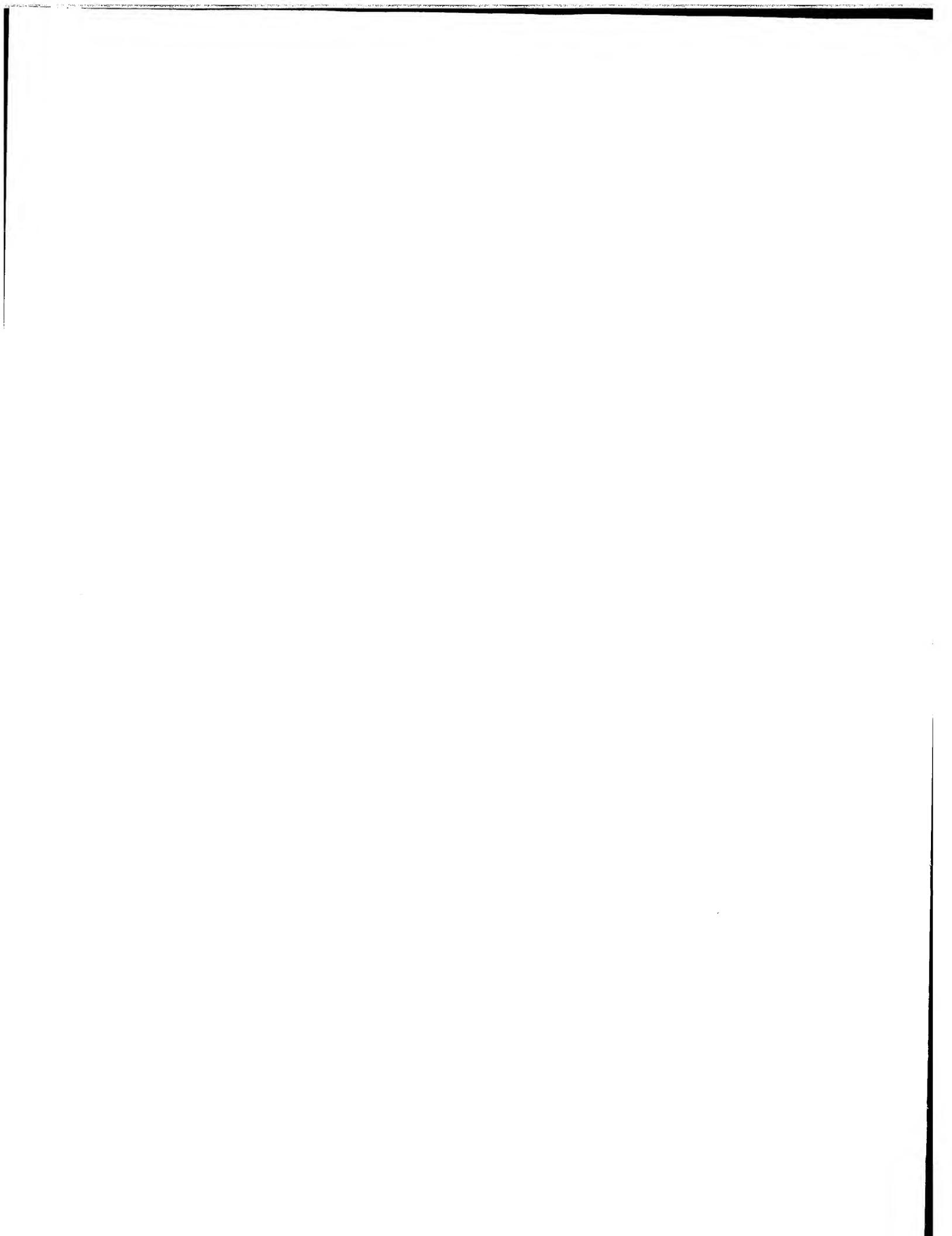
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COOLING MODULE AND REACTOR FOR CARRYING OUT AN EXOTHERMIC REACTION

The present invention relates to a cooling module and a reactor for carrying out an exothermic reaction comprising such a cooling module. In particular, the invention relates to a cooling module and reactor suitable for use in Fischer-Tropsch reactions.

The Fischer-Tropsch process is often used for the conversion of hydrocarbonaceous feed stocks into liquid and/or solid hydrocarbons. The feed stock (e.g. natural gas, associated gas, coal-bed methane and/or coal) is converted in a first step into a mixture of hydrogen and carbon monoxide (this mixture is often referred to as synthesis gas). The synthesis gas is then converted in a second step over a suitable catalyst at elevated temperature and pressure into paraffinic compounds ranging from methane to high molecular weight molecules comprising up to 200 carbon atoms, or, under particular circumstances, even more.

Numerous types of reactor systems have been developed for carrying out the Fischer-Tropsch reaction. For example, Fischer-Tropsch reactor systems include fixed bed reactors, especially multi tubular fixed bed reactors; fluidised bed reactors, such as entrained fluidised bed reactors and fixed fluidised bed reactors, and slurry bed reactors such as three-phase slurry bubble columns and ebulated bed reactors.

The Fischer-Tropsch reaction is very exothermic and temperature sensitive with the result that careful

temperature control is required to maintain optimum operation conditions and desired hydrocarbon product selectivity. Bearing in mind the very high heat of reaction which characterises the Fischer-Tropsch reaction 5 the heat transfer characteristics and cooling mechanisms of a reactor are very important.

The heat transfer performance of fixed-bed reactors is limited because of the relatively low mass velocity, small particle size and low thermal capacity of fluids. 10 If one attempts, however, to improve the heat transfer by increasing the gas velocity, a higher CO conversion can be obtained, but there is an excessive pressure drop across the reactor, which limits commercial viability. Increasing reactor capacity by increasing gas throughput 15 and CO conversation may result in increasing radial temperature gradients. For thermal stability and efficient heat removal the Fischer-Tropsch fixed-bed reactor tubes should have a diameter of less than 5 or 7 cm. The desired use of high-activity catalysts in 20 Fischer-Tropsch fixed-bed reactors makes the situation even worse. The poor heat transfer characteristics make local runaways (hotspots) possible, which may result in local deactivation of the catalyst. In order to avoid runaway reaction the maximum temperature within the 25 reactor must be limited. However, the presence of temperature gradients within the reaction mixture means that much of the catalyst is operating at sub-optimal levels.

The use of liquid recycle as a means of improving the 30 overall performance in a fixed-bed design has been described. Such a system is also called a "trickle bed" reactor (as part of a sub set of fixed-bed reactor systems) in which both reactant gas and liquid are

introduced (preferably in a down flow orientation with respect to the catalyst) simultaneously. The presence of the flowing reactant gas and liquid improves heat removal and heat control thus enhancing the reactor performance with respect to CO conversion and product selectivity. A limitation of the trickle bed system (as well as of any fixed-bed design) is the pressure drop associated with operating at high mass velocities. The gas-filled voidage in fixed-beds (typically less than 0.50) and size and shape of the catalyst particles does not permit high mass velocities without excessive pressure drops.

Consequently, the mass throughput undergoing conversion per unit reactor volume is limited due to the heat transfer rates. Increasing catalyst particle size and higher mass flow rates improve heat transfer (for a given pressure drop) and enable increased conversion capacity. However, the loss of catalyst selectivity and lower catalyst efficiency may offset the improved conversion capacity.

Three-phase slurry bubble column reactors generally offer advantages over the fixed-bed design in terms of heat transfer characteristics. Such reactors typically incorporate small catalyst particles suspended by upward flowing gas in a liquid continuous matrix. In the case of multi-tubular reactors, the number of tubes incorporated is generally limited by mechanical parameters. The motion of the continuous liquid matrix allows sufficient heat transfer to achieve a high commercial productivity. The catalyst particles are moving within a liquid continuous phase, resulting in, efficient transfer of heat generated from catalyst particles to the cooling surfaces, while the large liquid inventory in the reactor provides a high

thermal inertia, which helps prevent rapid temperature increases that can lead to thermal runaway.

Commercial fixed-bed and three-phase slurry reactors typically utilise boiling water to remove the heat of reaction. In the fixed-bed design, individual reactor tubes are located within a shell containing water/steam typically fed via flanges in the shell wall. The heat of reaction raises the temperature of the catalyst bed within each tube. This thermal energy is transferred to the tube wall forcing the water in the surrounding jacket to boil. In the slurry design, cooling tubes are placed within the slurry volume and heat is transferred from the liquid continuous matrix to the tube walls. The production of steam within the tubes provides the needed cooling. The steam in turn is used for heating purposes or to drive a steam turbine.

Synthesis gas leaking into the cooling system (identifiable through analysis of the steam output) cannot be separated, represents a risk and will force shutdown and repair of the slurry reactor. In light of the exothermic nature of the reaction and the typical volume of slurry reactors the shutdown process is both time consuming and expensive in terms of loss of production capacity. Where a reactor utilises a single header with multiple interconnected tubes the identification and repair of a leaking tube is difficult. In light of these difficulties it is known to block off a leaking tube rather than to attempt repair. However, blocking off a relatively large number of leaking tubes has the disadvantage of reducing cooling capacity resulting in a part of the reactor being uncooled, or under cooled, with the possible formation of hotspots.

Another drawback of known slurry reactors is that the cooling tubes are fixed in place inside the reactor during construction. Typically the cooling tubes are welded to headers through which the tubes are fed with coolant. Such an arrangement involves dangers for personnel during inspection and repair of individual cooling tubes when the reactor is configurated for use. Furthermore, given their large size, commercial reactors generally have to be transported in a horizontal position. This leads to difficulties in ensuring that tubes within the reactors are not damaged or dislodged.

It is one object of the present invention to provide a cooling module for use in an exothermic reaction reactor which is simple and efficient to construct, transport and operate, and which addresses some of the disadvantages described above in relation to cooling systems employed in known reactors.

It is another object of the invention to provide a cooling module that simplifies the identification and repair of leaks.

It is a further object of the invention to provide a reactor for carrying out an exothermic reaction having a cooling system which addressed the disadvantages described above in relation to known reactors.

Accordingly the present invention provides a removable cooling module having first and second ends, for use in a reactor for carrying out an exothermic reaction, the cooling module comprising:

- 30 a coolant feed tube;
- a distribution chamber;
- a plurality of circulation tubes; and
- a collection chamber;

said coolant feed tube having at its first end an inlet, for charging the cooling module with coolant, and communicating with said distribution chamber at its second end;

5 each of said circulation tubes communicating with the distribution chamber through a first end and communicating with said collection chamber through a second end;

10 the collection chamber having an outlet for discharging coolant; wherein the inlet and the outlet are both located towards the same end of the cooling module.

15 Preferably the inlet is adapted to be removably connectable to a charge pipe and the outlet is adapted to be removably connectable to a discharge pipe.

Preferably the distribution chamber comprises a conical section defining apertures through which the distribution chamber communicates with each of the circulation tubes.

20 Preferably the collection chamber comprises a conical section defining apertures through which the collection chamber communicates with each of the circulation tubes.

25 In a preferred embodiment the coolant feed tube is located substantially centrally with respect to the distribution tubes and may optionally protrude through the collection chamber.

30 The cooling module may comprise any number of circulation tubes required to provide sufficient cooling that is preferably between about 20 and about 4,000 circulation tubes and more preferably between about 100 and about 400.

According to another aspect, the invention provides a reactor for carrying out an exothermic reaction, said reactor comprising:

a reactor shell;

5 means for introducing reactants into the reactor shell;

means for removing products from the reactor shell;

and

cooling means;

10 wherein said cooling means comprises at least one cooling module as described above.

Preferably the reactor shell comprises access means, such as a manhole, for accessing the cooling means.

15 Preferably the reactor comprises support means for supporting the cooling means.

Typically the means for introducing reactants into the reactor shell may comprise a sparger for introducing syngas.

20 Typically the means for removing products from the reactor shell may comprise a filter.

Preferably the reactor further comprises one or more screens or baffles adapted to modify the circulation of reactants and products within the reactor shell.

25 For each cooling module, in use, the inlet is typically removably connected to a charge pipe and each outlet is typically removably connected to a discharge pipe.

30 Preferably the connection between the inlet and the charge pipe is achieved by means of an inlet flange and a charge pipe flange secured with a 'c-clamp' or other suitable fixing means. Similarly, the connection between the outlet and the discharge pipe is preferably achieved

by means of an outlet flange and a discharge pipe flange secured with a 'c-clamp' or other suitable fixing means.

5 The modular nature of the cooling system has the advantage that individual cooling modules may be removed from the reactor shell, for example for inspection, replacement, maintenance or repair purposes. Furthermore, the reactor shell and cooling modules may be manufactured and transported separately. Additional advantages of the cooling module and the reactor of the present invention 10 will be apparent from the detailed description below.

According to a further aspect, the invention provides a method for carrying out an exothermic reaction comprising the steps of:

15 charging a reactor with reactants;
cooling the contents of the reactor; and
removing products from the reactor,
wherein the cooling step is carried out using cooling means comprising at least one cooling module as described above.

20 According to a still further aspect, there is provided a process for the synthesis of hydrocarbons using a reactor of the type provided by the present invention.

25 Without wishing to be restricted to a particular embodiment, the invention will now be described in further detail with reference to the drawings in which:

Figure 1 depicts a vertical cross-section through a cooling module according to the invention;

30 Figure 2 illustrates a number of cooling modules in a reactor;

Figure 3 is a plan view of a reactor housing a plurality of cooling modules;

Figure 4 is an elevation of the inlet/outlet piping arrangement at the top of a cooling module; and

Figure 5 illustrates the support of a cooling module at the base of a reactor.

5 Turning now to Figure 1 a first embodiment of a cooling module 1 according to the invention comprises a coolant feed tube 2, for introducing a coolant into the module, having an inlet 3 at its first end and being in fluid communication with a distribution chamber 4 located at its second end. The distribution chamber 4 is in turn in fluid communication with one or more circulation tubes 5 through a first end of each of said tubes 5, with the second end of each circulation tube 5 communicating with a collection chamber 6. The collection chamber 6 has an outlet 7 for discharging the coolant. The direction of flow of coolant within the cooling module 1 is indicated with arrows. The configuration of the cooling module 1 is such that the inlet 3 and outlet 7 are located adjacent to each other towards the same end of the cooling module.

10 In operation the inlet 3 is removably connected to a charge pipe 8 and the outlet 7 is removably connected to a discharge pipe 9. Preferably, removable connection of the charge pipe 8 to the inlet 3 may be provided by means of charge pipe flange 8a and inlet flange 3a which may be removably sealed using a 'C'-clamp (not shown) or suitable means. Similarly, removable connection of the discharge pipe 9 to the outlet 7 may be provided by means of discharge pipe flange 9a and outlet flange 7a which may be removably sealed using a 'C'-clamp (not shown) or the like.

15 In principle removable connection may be achieved by welding together the components in question, wherein they may be disconnected by suitable cutting means.

Coolant is introduced through charge pipe 6 into the cooling module 1 via inlet 3 and flows through coolant feed tube 2 to the distribution chamber 4. The coolant is then distributed through circulation tubes 5 to 5 collection chamber 6 where it is collected and discharged via outlet 7 and discharge pipe 7. Heat is transferred from the slurry surrounding the cooling module 1 to the coolant as it passes through the module and in particular as the coolant flows through the circulation tubes 5 and, 10 to a lesser extent, the coolant feed tube 2.

Preferably the cooling module 1 is configured such that the inlet 3 and outlet 7 are located relatively close to each other, thus providing ease of access.

Suitable coolants will be known to the person skilled 15 in the art and include for example water/steam or oil based coolants.

Any configuration of coolant feed tube 2, distribution chamber 4, circulation tubes 5 and collection chamber 6 which provides effective cooling may 20 be employed. Preferably the coolant feed tube 2 is located substantially centrally with respect to the circulation tubes 5 as shown in Figure 1. Such a configuration enhances mechanical stability of the cooling module 1 and facilitates distribution and 25 collection of the coolant. In the embodiment shown in Figure 1 the coolant feed tube 2 protrudes through the collection chamber 4. The distribution chamber 4 and collection chamber 6 may be of any shape which facilitates efficient distribution and collection of 30 coolant within the module 1. For example, the distribution chamber 4 and the collection chamber 6 may be spherical or curved (hemispherical) in nature. It is preferable to avoid flat surfaces, particularly in

relation to the distribution chamber 4, where catalyst particles in the slurry surrounding the cooling module may accumulate. It is envisaged that the circulation tubes 5 may be connected directly to the lower end of the coolant feed tube 2, in which case the lower end (that is to say the end furthest from the inlet 3) of the coolant feed tube 2 represents a distribution chamber. It is preferred that the distribution chamber 4 and the collection chamber 6 each comprise a conical section through which each of said chambers 4, 6 communicate with respective ends of the circulation tubes 5. Preferably the distribution chamber 4 and the collection chamber 6 each comprise a conical section the curved surface of which defines an angle of between 0 and about 45° to the vertical. Clearly, in the case where this angle is 0° the circulation tubes 5 are connected directly to the lower end (that is to say the end furthest from the inlet 3) of the coolant feed tube 2.

The cooling module characteristically comprises a plurality of elongated circulation tubes 5 which facilitate circulation of coolant within the module 1. The circulation tubes 5 are preferably substantially parallel to and equidistant from each other.

The number and size of circulation tubes 5 in the cooling module 1 is limited only by the cooling requirements of particular circumstances and physical constraints of manufacture. Typically a cooling module will comprise between about 10 and about 4,000 circulation tubes, preferably between about 100 and about 400. Depending on the volume and capacity of the reactor, each cooling tube may be about 4 to about 40 m in length. Preferably the cooling tubes (5) are from about 10 to about 25 m in length. The circulation tubes

usually comprise a bundle of elongated, parallel, straight tubes. Preferably the feed tube is also an elongated, straight tube, preferably parallel with the circulation tubes. While maintaining strength and 5 physical integrity under the operating conditions of the reactor, the cooling tubes are preferably as thin as possible in order to facilitate efficient heat transfer and to minimise the overall weight of the cooling module 1. In order to maximise the reaction volume within 10 a reactor the diameter of each circulation tube should be as small as possible, for example, from about 1 to about 10 cm, preferably from about 2 to about 5cm.

The shape, size and configuration of the cooling 15 modules and their arrangement within a reactor will be governed primarily by factors such as the capacity, operating conditions and cooling requirements of the reactor. The cooling module may have any cross section which provides for efficient packing of cooling modules within a reactor, for example, the cooling module may be 20 of square, rectangular or hexagonal cross section. A cooling module design that incorporates a square cross section is advantageous in terms of packing the modules within the reactor and in providing uniform cooling throughout the reactor volume. The cross sectional area 25 of the cooling module may typically be about 0.20 to 2.00 m² depending upon the number and configuration of cooling tubes employed and the cooling capacity required.

Figure 2 illustrates one particular embodiment of another aspect of the invention, namely, a reactor 20 for 30 carrying out an exothermic reaction. The reactor 20 comprises a reactor shell 21, reactant inlet means (not shown), product outlet means (not shown) and a cooling system comprising a plurality of cooling modules 1 as

described above. Each cooling module 1 is removably held in place using suitable means. For example, supports 23 may be incorporated into the bottom of the reactor 20. Further means (not shown) may be provided at or towards the top of each cooling module 1 in order to ensure that they remain in the correct position within the reactor 20.

Access means, for example a manhole 22, provides access to the interior of the reactor 20 and specifically to cooling modules 1. The shape and size of the access means will be determined primarily by the dimensions of the internal components. Preferably a manhole having a diameter of between about 0.5 and about 3.0 m may be incorporated into the reactor shell 21, provided that this is compatible with the dimensions of the cooling modules 1 employed.

In known reactors cooling tubes are typically welded into place during manufacture. Given the size of commercial scale slurry reactors it is normally not possible to transport them in a vertical position. Transporting such a reactor horizontally places considerable strain on the cooling tubes inside the shell which can lead to the tubes being damaged during transportation. Thus the modular design of the cooling system of the invention represents a considerable advantage in that the cooling modules 1 and the reactor shell 21 may be manufactured and transported separately for assembly at the desired site. Furthermore the cooling modules 1 may be lowered into position in the reactor shell 21 without the need for any personnel to be inside at the bottom of the reactor. This eliminates the hazards associated with personnel having to operate within the reactor as is the case where cooling tubes have to be

welded in place (for example, welded to a tube sheet or header located at the bottom of the reactor shell).

During construction, when a reactor is typically lying in a horizontal position, suitable means may be employed to support the cooling modules. For example one or more diaphragms or support grids may be positioned between the cooling modules or indeed between the circulation tubes 5 of each module 1. Such support means may optionally be left in place during operation of the reactor in order to maintain spacing between the elements in question and in particular to support the circulation tubes relative to each other.

Typically the charge pipe 8 and discharge pipe 9 are removably connectable to charge and discharge conduits 24, 25 which pass through the reactor shell 21 and may be connected to elements external of the reactor. The charge and discharge pipes 8, 9 may be connected to the charge and discharge conduits 24, 25 using 'c-clamps', as described above, or other suitable means.

Figure 4 illustrates, the removable connections between charge pipe 8 and inlet 3, discharge pipe 9 and outlet 7, charge pipe 8 and charge conduit 24, and discharge pipe 9 and discharge conduit 25 thus facilitating separate removal of each individual cooling module 1 from the reactor shell 21. Figures 2, 3 and 4 illustrate that once the connections referred to in the previous sentence have all been removed, the charge pipe 8 and discharge pipe 9 may be moved thus allowing for the cooling module 1 to be lifted vertically from its support 23. External lifting means (not shown) located above the reactor 20 may be attached, through the manhole 22 to a lifting fixture (not shown) on the cooling module 1.

With particular reference to Figure 3 it will be appreciated that, once disconnected, the central-most cooling module may be lifted directly out of the reactor 20 via the manhole 22. The space vacated by the central-most module facilitates shuffling or movement of the remaining cooling modules 1 within the reactor shell 21. Internal lifting means (not shown) such as a hoist fixed in a space between the top of the cooling modules 1 and the ceiling of the reactor shell 21 may be provided to facilitate shuffling of the modules.

Figure 5 illustrates the arrangement at the bottom of a reactor shell 21 wherein supports 23 may be provided to bear the weight of each cooling module 1. The supports 23 further serve to maintain the position of each cooling module 1 within the reactor 20. The end of a module 1 received by a support 23 is preferably adapted so that the cooling module 1 may be lowered into position from above without the need for any personnel to be present in the reactor. This represents an additional safety feature of the present invention.

As described above, synthesis gas leaking into the cooling system can be identified through analysis of the discharged coolant. In known reactors the repair of leaking cooling tubes can be difficult and in some cases not possible at all, in which case the leaking tube may have to be blocked off rather than repaired. Blocking off cooling tubes causes undesirable reductions in cooling capacity and can lead to unwanted hot spots or run away reaction in areas of the reaction mixture which are not properly cooled.

The present invention provides a cooling unit that can be employed in modular system whereby individual cooling units 1 can be isolated and separately removed

from the reactor 20 for inspection, replacement or repair purposes. This modular approach has the further advantage that repair of a leaking cooling module can be carried out outside of the reactor shell, thus eliminating the 5 risks associated with the need for personnel to enter the reactor in order to effect repairs. The present invention facilitates straightforward and rapid repair of cooling modules, resulting in shorter down time than for that associated with repair of known reactors, with the 10 advantage that lost production time can be minimised.

Typically the reactor may be used for carrying out three phase slurry reactions, such as for example Fisher Tropsch type reactions. The reactant inlet means may comprise one or more spargers located at the base of the 15 reactor shell 21 and the product outlet means may comprise one or more filters. The person skilled in the art will be familiar with suitable sparger and filter systems employed in known three-phase slurry reactors.

The average particle size of the catalyst particles 20 may vary between wide limits, depending inter alia on the type of slurry zone regime. Typically, the average particle size may range from 1 μm to 2 mm, preferably from 1 μm to 1 mm.

If the average particle size is greater than 100 μm , 25 and the particles are not kept in suspension by a mechanical device, the slurry zone regime is commonly referred to as ebullating bed regime. Preferably, the average particle size in an ebullating bed regime is less than 600 μm , more preferably in the range from 100 to 30 400 μm . It will be appreciated that in general the larger the particle size of a particle, the smaller the chance that the particle escapes from the slurry zone into the freeboard zone. Thus, if an ebullating bed regime is

employed, primarily fines of catalyst particles will escape to the freeboard zone.

If the average particle size is at most 100 μm , and the particles are not kept in suspension by a mechanical device, the slurry zone regime is commonly referred to as a slurry phase regime. Preferably, the average particle size in a slurry phase regime is more than 5 μm , more preferably in the range from 10 to 75 μm .

If the particles are kept in suspension by a mechanical device, the slurry zone regime is commonly referred to as stirred tank regime. It will be appreciated that in principle any average particle size within the above ranges can be applied. Preferably, the average particle size is kept in the range from 1 to 200 μm .

The concentration of catalyst particles present in the slurry may range from 5 to 45% by volume, preferably, from 10 to 35% by volume. It may be desired to add in addition other particles to the slurry, as set out in for example European Patent Application Publication

No. 0 450 859. The total concentration of solid particles in the slurry is typically not more than 50% by volume, preferably not more than 45% by volume.

Suitable slurry liquids are known to those skilled in the art. Typically, at least a part of the slurry liquid is a reaction product of the exothermic reaction. Preferably, the slurry liquid is substantially completely a reaction product.

The exothermic reaction is a reaction which is carried out in the presence of a solid catalyst, and which is capable of being carried out in a three-phase slurry reactor. Typically, at least one of the reactants of the exothermic reaction is gaseous. Examples of

exothermic reactions include hydrogenation reactions, hydroformylation, alkanol synthesis, the preparation of aromatic urthanes using carbon monoxide, Kölbel-
5 Engelhardt synthesis, polyolefin synthesis, and Fischer-Tropsch synthesis. According to a preferred embodiment of the present invention, the exothermic reaction is a Fischer-Tropsch synthesis reaction.

10 The Fischer-Tropsch synthesis is well known to those skilled in the art and involves synthesis of hydrocarbons from a gaseous mixture of hydrogen and carbon monoxide, by contacting that mixture at reaction conditions with a Fischer-Tropsch catalyst.

15 Products of the Fischer-Tropsch synthesis may range from methane to heavy paraffinic waxes. Preferably, the production of methane is minimised and a substantial portion of the hydrocarbons produced have a carbon chain length of a least 5 carbon atoms. Preferably, the amount of C₅+ hydrocarbons is at least 60% by weight of the total product, more preferably, at least 70% by weight, even more preferably, at least 80% by weight, most preferably at least 85% by weight. Reaction products which are liquid phase under reaction conditions may be separated and removed using suitable means, such as one or more filters. Internal or external filters, or a 20 combination of both, may be employed. Gas phase products such as light hydrocarbons and water may be removed using suitable means known to the person skilled in the art.

25 Fischer-Tropsch catalysts are known in the art, and typically include a Group VIII metal component, preferably cobalt, iron and/or ruthenium, more preferably cobalt. Typically, the catalysts comprise a catalyst carrier. The catalyst carrier is preferably porous, such

as a porous inorganic refractory oxide, more preferably alumina, silica, titania, zirconia or mixtures thereof.

5 The optimum amount of catalytically active metal present on the carrier depends inter alia on the specific catalytically active metal. Typically, the amount of cobalt present in the catalyst may range from 1 to 100 parts by weight per 100 parts by weight of carrier material, preferably from 10 to 50 parts by weight per 100 parts by weight of carrier material.

10 The catalytically active metal may be present in the catalyst together with one or more metal promoters or co-catalysts. The promoters may be present as metals or as the metal oxide; depending upon the particular promoter concerned. Suitable promoters include oxides of metals from Groups IIA, IIIB, IVB, VB, VIB and/or VIIB of the Periodic Table, oxides of the lanthanides and/or the actinides. Preferably, the catalyst comprises at least one of an element in Group IVB, VB and/or VIIB of the Periodic Table, in particular titanium, zirconium, 15 maganese and/or vanadium. As an alternative or in addition to the metal oxide promoter, the catalyst may comprise a metal promoter selected from Groups VIIB and/or VIII of the Periodic Table. Preferred metal promoters include rhenium, platinum and palladium.

20 25 A most suitable catalyst comprises cobalt as the catalytically active metal and zirconium as a promoter. Another most suitable catalyst comprises cobalt as the catalytically active metal and maganese and/or vanadium as a promoter.

30 The promoter, if present in the catalyst, is typically present in an amount of from 0.1 to 60 parts by weight per 100 parts by weight of carrier material. It will however be appreciated that the optimum amount of

promoter may vary for the respective elements which act as promoter. If the catalyst comprises cobalt as the catalytically active metal and manganese and/or vanadium as promoter, the cobalt : (manganese + vanadium) atomic ratio is advantageously at least 12:1.

5 The Fischer-Tropsch synthesis is preferably carried out at a temperature in the range from 125 to 350 °C, more preferably 175 to 275 °C, most preferably 200 to 260 °C. The pressure preferably ranges from 5 to 10 150 bar abs., more preferably from 5 to 80 bar abs.

Hydrogen and carbon monoxide (synthesis gas) is typically fed to the three-phase slurry reactor at a molar ratio in the range from 0.4 to 2.5. Preferably, the hydrogen to carbon monoxide molar ratio is in the range 15 from 1.0 to 2.5.

20 The gaseous hourly space velocity may vary within wide ranges and is typically in the range from 1500 to 10000 Nl/l/h, preferably in the range from 2500 to 7500 Nl/l/h.

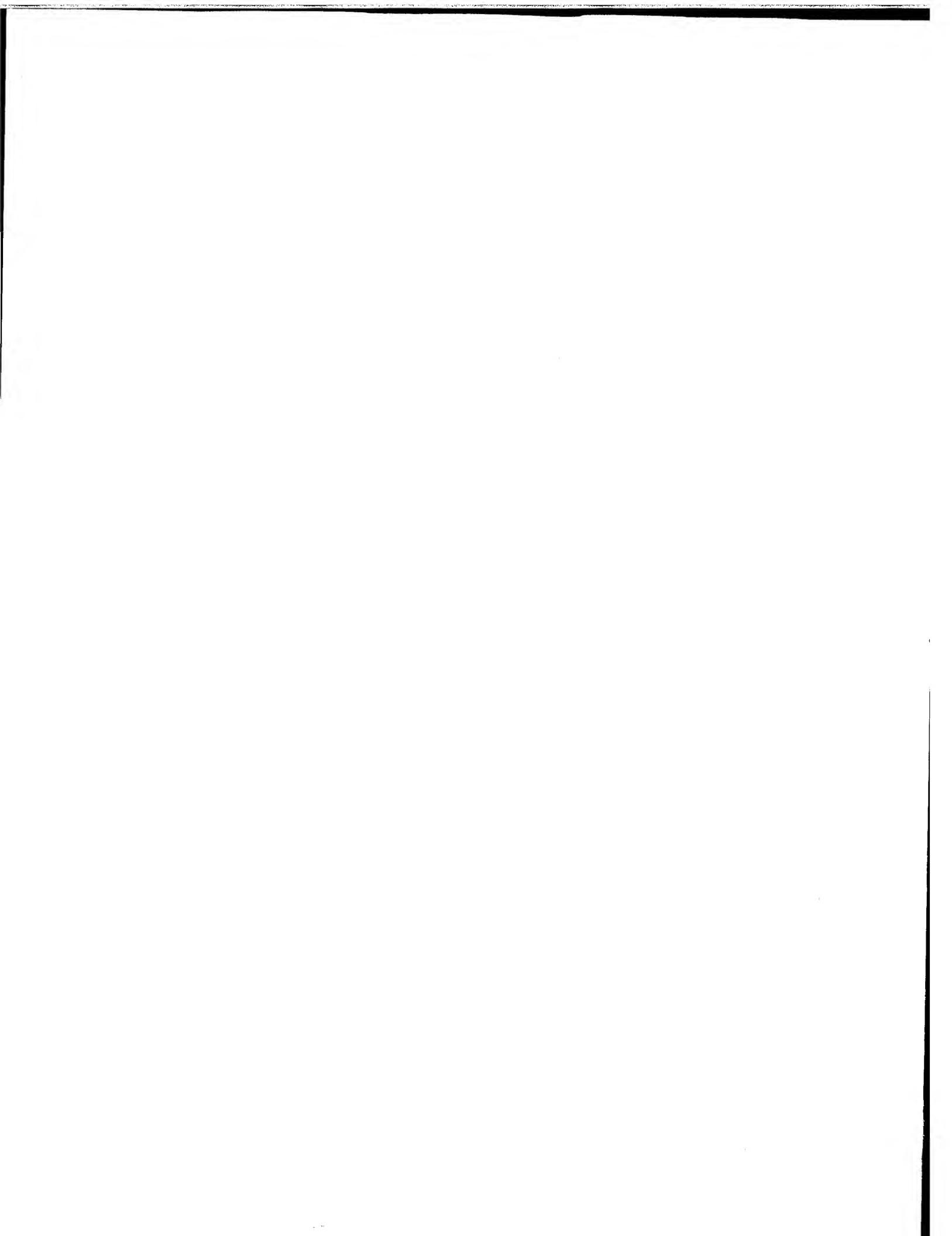
The Fischer-Tropsch synthesis is preferably carried 25 out in a slurry phase regime or an ebullating bed regime, wherein the catalyst particles are kept in suspension by an upward superficial gas and/or liquid velocity.

It will be understood that the skilled person is 25 capable to select the most appropriate conditions for a specific reactor configuration and reaction regime.

Preferably, the superficial gas velocity of the synthesis gas is in the range from 0.5 to 50 cm/sec, more preferably in the range from 5 to 35 cm/sec.

30 Typically, the superficial liquid velocity is kept in the range from 0.001 to 4.00 cm/sec, including liquid production. It will be appreciated that the preferred range may depend on the preferred mode of operation.

According to one preferred embodiment, the superficial liquid velocity is kept in the range from 0.005 to 1.0 cm/sec.





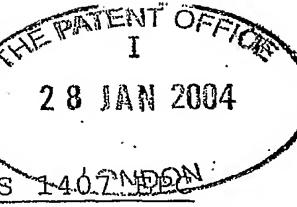
C L A I M S

1. A removable cooling module (1) having first and second ends, for use in a reactor (20) for carrying out an exothermic reaction, the cooling module comprising a coolant feed tube (2); a distribution chamber (4); a plurality of circulation tubes (5); and a collection chamber (6); said coolant feed tube (2) having at its first end an inlet (3), for charging the coolant module (1) with coolant, and communicating with said distribution chamber (4) at its second end; each of said circulation tubes (5) communicating with the distribution chamber (4) through a first end and communicating with said collection chamber (6) through a second end; the collection chamber (6) having an outlet (7) for discharging coolant; wherein the inlet (3) and the outlet (7) are both located towards the same end of the cooling module (1).
2. A cooling module according to claim 1 wherein the inlet (3) is adapted to be removably connectable to a charge pipe (8) and the outlet (7) is adapted to be removably connectable to a discharge pipe (9).
3. A cooling module according to either of claims 1 and 2 wherein the second end of the coolant feed tube (2) represents a distribution chamber (4) with the circulation tubes (5) connected thereto.
- 25 4. A cooling module according to either of claims 1 and 2 wherein the distribution chamber (4) comprises a conical section defining apertures through which the distribution chamber (4) communicates with each of the circulation tubes (5).

5. A cooling module according to claim 4 wherein the distribution chamber comprises a conical section, the curved surface of which defines an angle of between 0 and about 45° to the vertical.
- 5 6. A cooling module according to any of the preceding claims wherein the collection chamber (6) comprises a conical section defining apertures through which the collection chamber (6) communicates with each of the circulation tubes (5).
- 10 7. A cooling module according to claim 6 wherein the collection chamber (6) comprises a conical section, the curved surface of which defines an angle of between 0 and about 45° to the vertical.
- 15 8. A cooling module according to any of the preceding claims wherein the coolant feed tube (2) is located substantially centrally with respect to the circulation tubes (5).
- 20 9. A cooling module according to claim 8 wherein the coolant feed tube (2) protrudes through the collection chamber (6).
10. A cooling module according to any of the preceding claims comprising between about 20 and about 4,000 circulation tubes (5).
- 25 11. A cooling module according to claim 10 comprising between about 100 and about 400 circulation tubes (5).
12. A cooling module according to any of the preceding claims wherein each of the cooling tubes (5) has a length of about 4 to about 40 metres.
- 30 13. A cooling module according to claim 12 wherein each of the circulation tubes (5) has a length of about 10 to about 25 metres.

14. A cooling module according to any of the preceding claims wherein the diameter of each circulation tube is from about 1 to about 10 cm.
- 5 15. A cooling module according to claim 14 wherein each of the cooling tubes (5) has a diameter of from about 2 to about 5 cm.
- 10 16. A cooling module according to any of the preceding claims having a square, rectangular or hexagonal cross section.
- 15 17. A cooling module according any of the preceding claims having a square cross sectional area of from about 0.20 to 2.00 m².
- 20 18. A reactor (20) for carrying out an exothermic reaction, said reactor (20) comprising a reactor shell (21); means for introducing reactants into the reactor shell (21); means for removing products from the reactor shell (21); and cooling means; wherein said cooling means comprises at least one cooling module (1) according to any of claims 1 to 17.
- 25 19. A reactor according to claim 18 wherein the reactor shell (21) comprises access means (22) for accessing the cooling means.
- 20 20. A reactor according to either of claims 18 and 19 further comprising support means (23) for supporting the cooling means.
- 30 21. A reactor according to any of claims 18 to 20 wherein the means for introducing reactants into the reactor shell (21) comprises a sparger.
22. A reactor according to any of claims 18 to 21 wherein the means for separating products from the reaction mixture (21) comprises a filter.
23. A reactor according to claim 22 comprising an internal filter located within the reactor shell (21).

24. A reactor according to either of claims 22 and 23 comprising an external filter located outside of the reactor shell (21).
25. A reactor according to any of claims 18 to 24 further comprising means adapted to modify the circulation of reactants and products within the reactor shell (21).
26. A method for carrying out an exothermic reaction comprising the steps of: charging a reactor (20) with reactants; cooling the contents of the reactor (20) and removing products from the reactor (20), wherein cooling is carried out using cooling means comprising at least one cooling module (1) according to Claims 1 to 17.
27. A process according to claim 26 for the synthesis of hydrocarbons wherein the reactor (20) is charged with syngas.
28. A product obtained according to the process of either of claims 26 and 27.

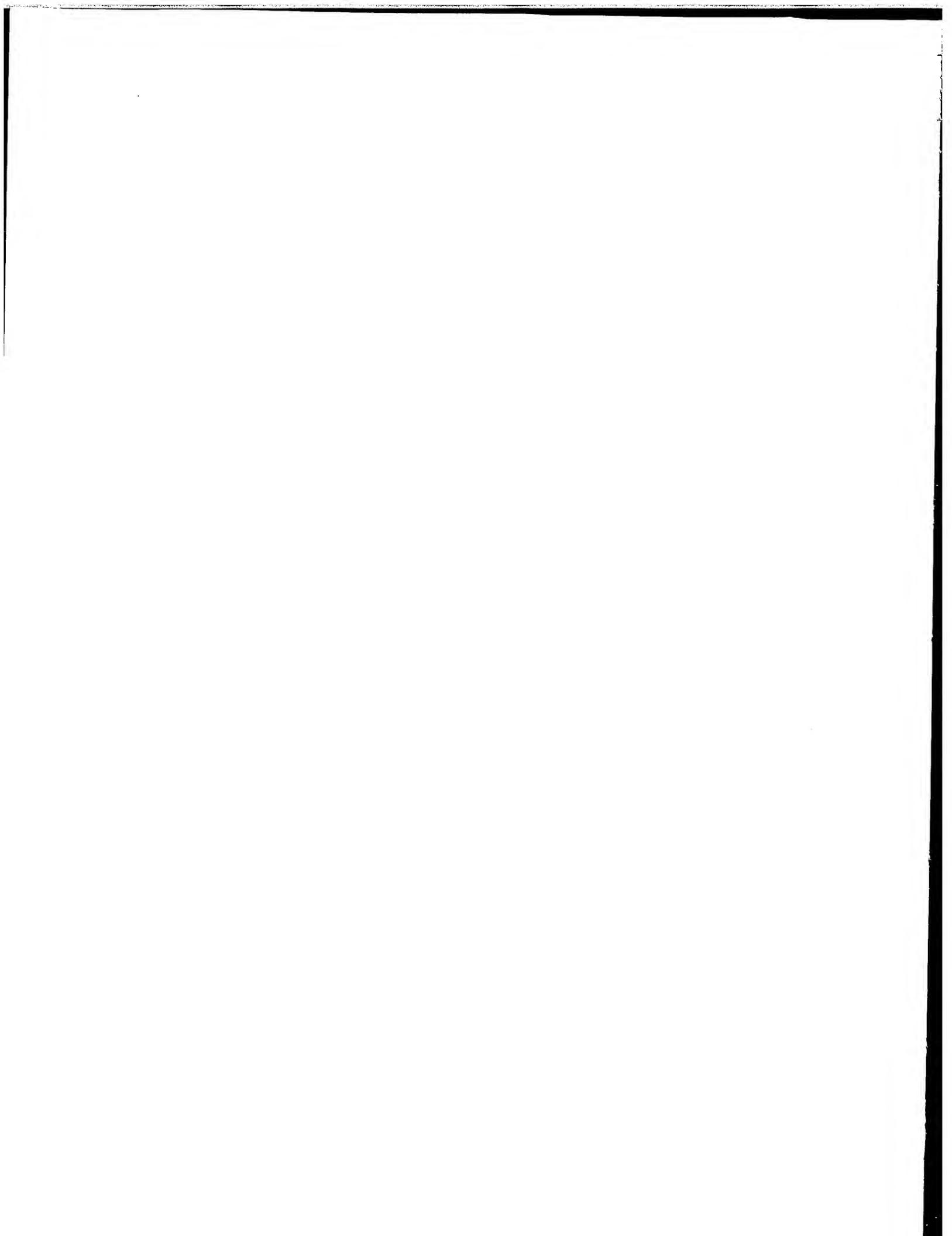


A B S T R A C T

COOLING MODULE AND REACTOR FOR CARRYING OUT AN EXOTHERMIC
REACTION

Disclosed is a removable cooling module (1), for use in a reactor (20) for carrying out an exothermic reaction, comprising a coolant feed tube (2); a distribution chamber (4); a plurality of circulation tubes (5); and a collection chamber (6); said coolant feed tube (2) having at its first end an inlet (3), for charging the coolant module (1) with coolant, and communicating with said distribution chamber (4) at its second end; each of said circulation tubes (5) communicating with the distribution chamber (4) through a first end and communicating with said collection chamber (6) through a second end; the collection chamber (6) having an outlet for discharging coolant. The modular nature of the invention facilitates removal of individual cooling modules (1) from a reactor shell (21).

(Fig. 2)



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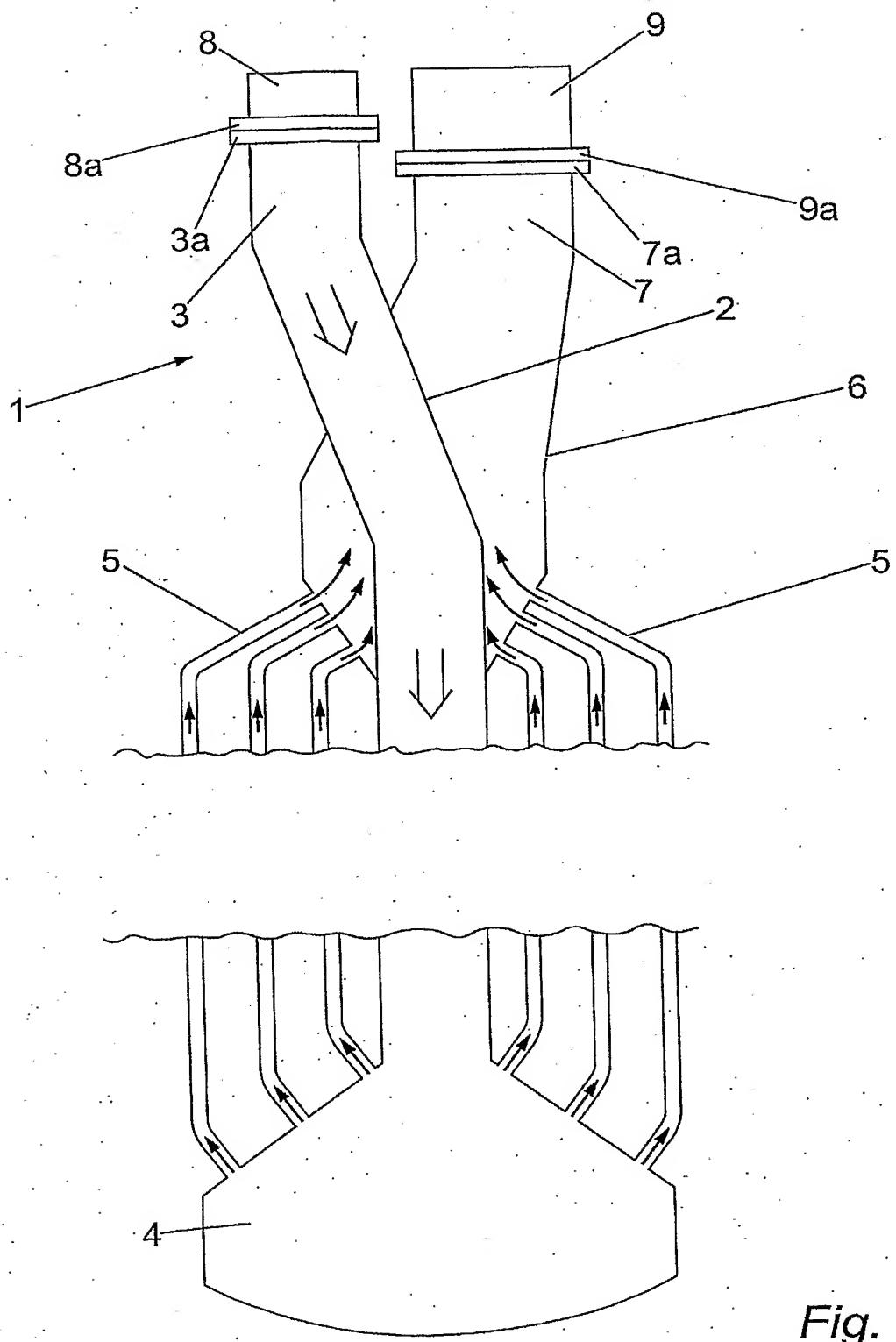


Fig. 1

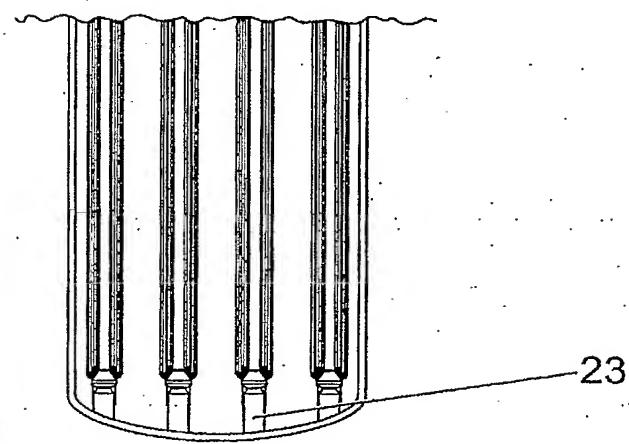
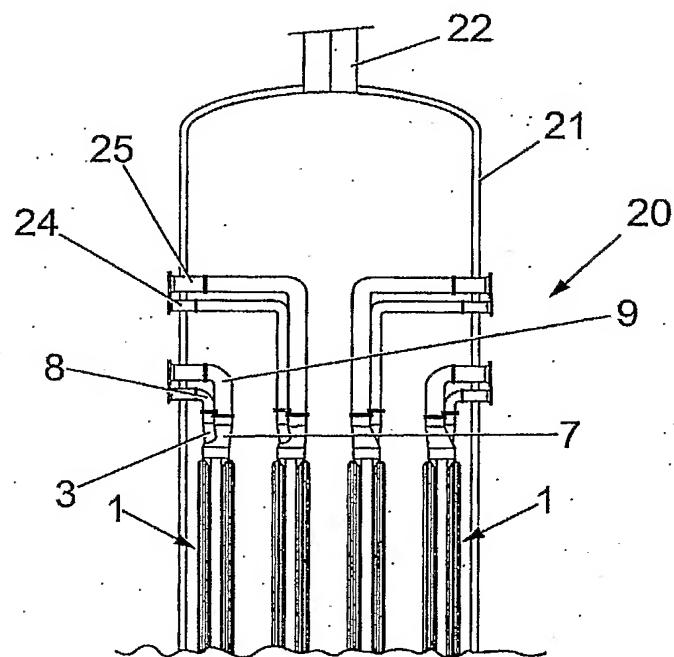


Fig. 2

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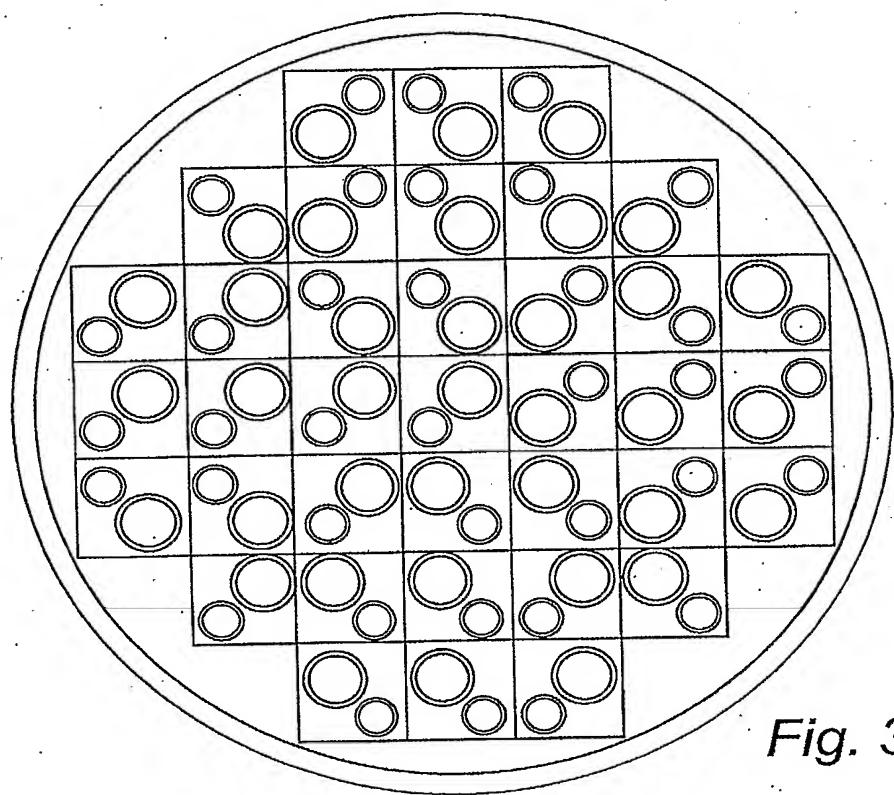


Fig. 3

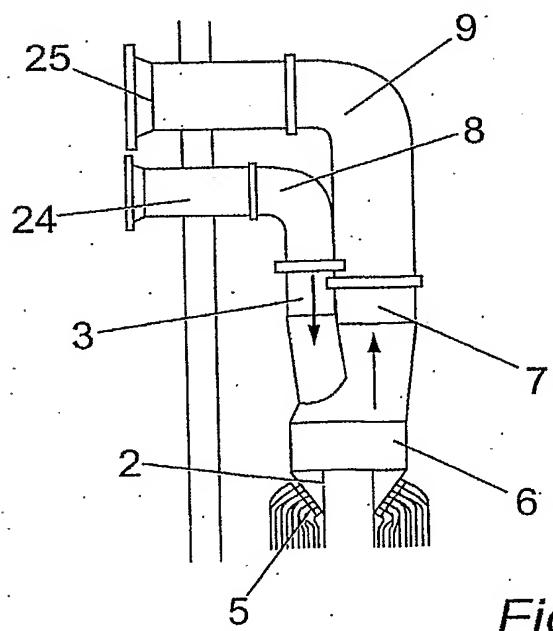


Fig. 4

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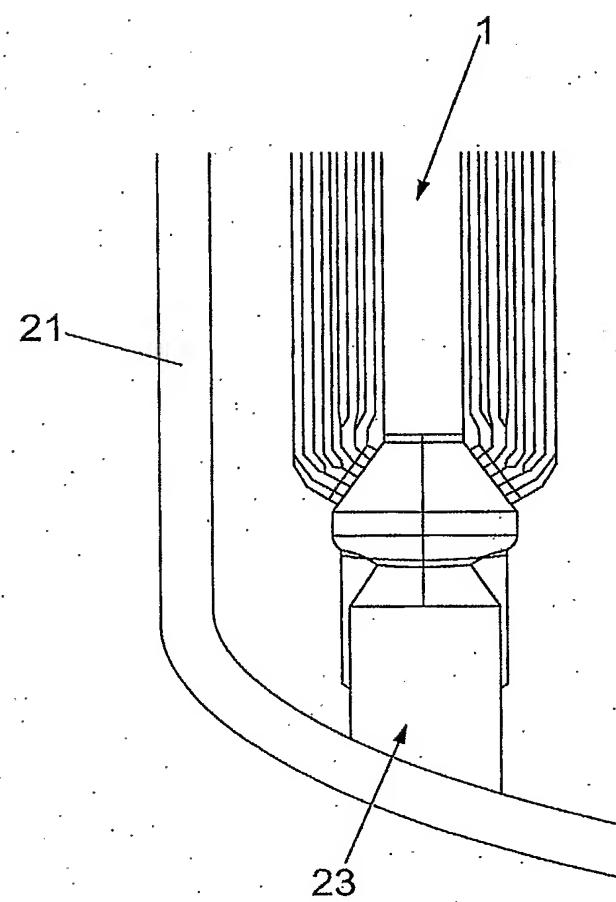


Fig. 5